

# Supplanting Gravity with Centrifugal Force for Sieving and Processing Regolith under Micro-Gravity

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# Why size-segregate regolith?

## Improve reliability of ISRU processing systems

- Remove size populations that foul seals
- Reduce mean particle size to improve system throughput of chemical processing systems

## Construction applications

- Size graded regolith would have different uses for different construction jobs: berms, road beds, habitat cover, etc...

## Manufacturing applications using regolith

- Sintering, additive manufacturing, etc... improved results with well defined particle size

# Low gravity has a negative impact on granular flow

- $\mu$ -g granular flows will act like a more cohesive flow compared to 1-g
- Larger openings required in low-g gravity driven flow
- Vibrational sieving does not function as well in low-g



**Table 3:** Summary of sieve runs in lunar-g trajectories

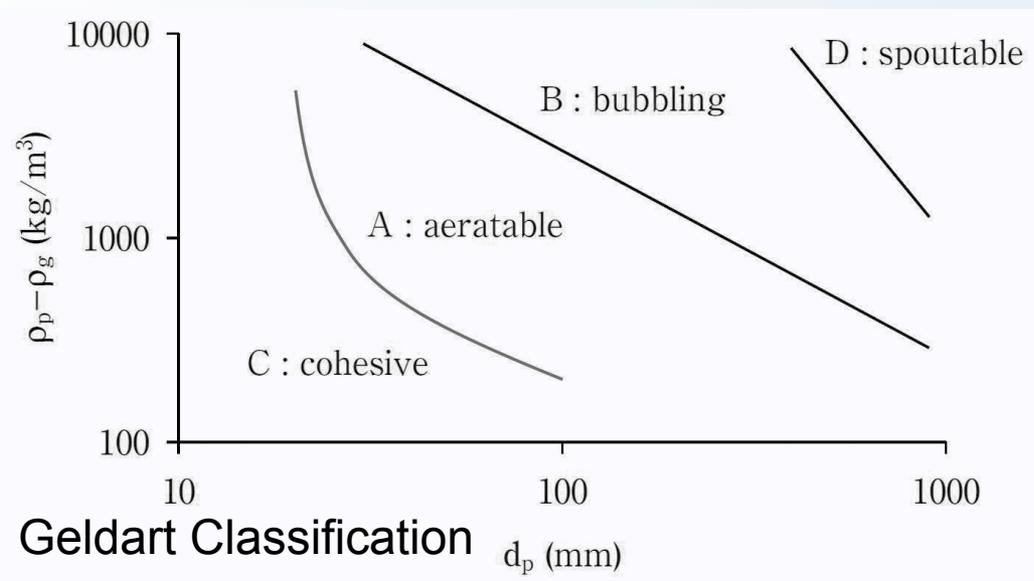
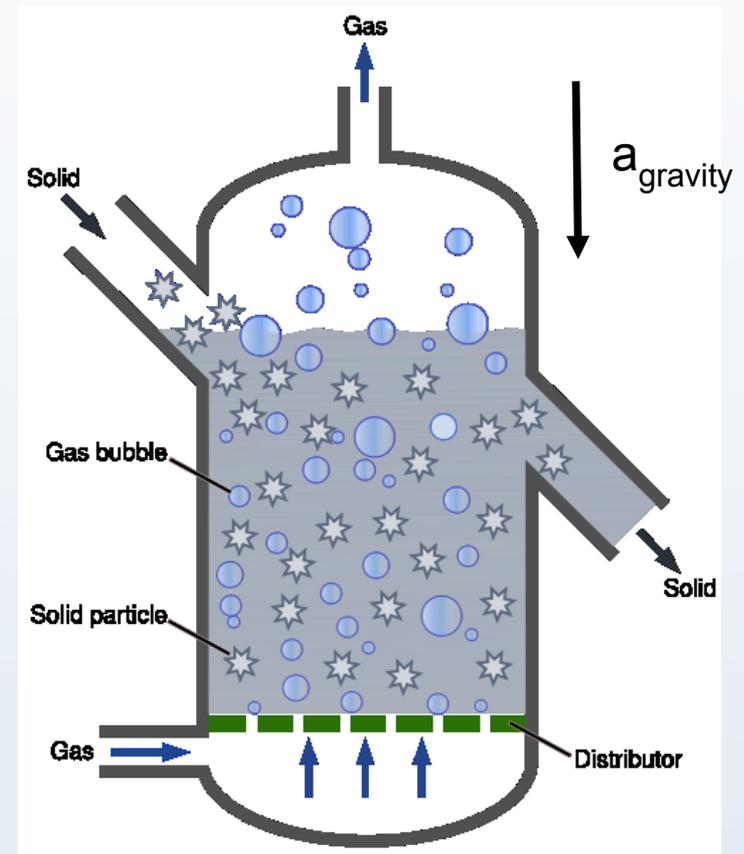
| Sieve ID | Simulant | Mesh size         | Initial mass | Passed mass | % Passing |
|----------|----------|-------------------|--------------|-------------|-----------|
| 1        | JSC1-a   | 75 $\mu\text{m}$  | 100 g        | 7.5 g       | 7.5       |
| 2        | LHT      | 150 $\mu\text{m}$ | 100 g        | 4.1 g       | 4.1       |
| 3        | LHT      | 500 $\mu\text{m}$ | 199.1 g      | 85.4 g      | 42.9      |
| 4        | LHT      | 75 $\mu\text{m}$  | 100.1 g      | 2.7 g       | 2.7       |
| 5        | LHT      | 150 $\mu\text{m}$ | 100 g        | 3.7 g       | 3.7       |
| 6        | LHT      | 500 $\mu\text{m}$ | 200 g        | 61.3 g      | 30.7      |
| 7        | LHT      | 75 $\mu\text{m}$  | 100 g        | 0.1 g       | 0.1       |
| 8        | JSC1-a   | 150 $\mu\text{m}$ | 100.1 g      | 15.3 g      | 15.3      |

Townsen et al. (2010)  
40<sup>th</sup> Aerospace  
Mechanisms Symposium  
NASA/CP-2010-216272

Ramé et al. (2010) "Flowing and Sifting Lunar Soil Simulant in Lunar Gravity" (Zero-G flights Aug 13-14, 2009, Final Report, GRC)

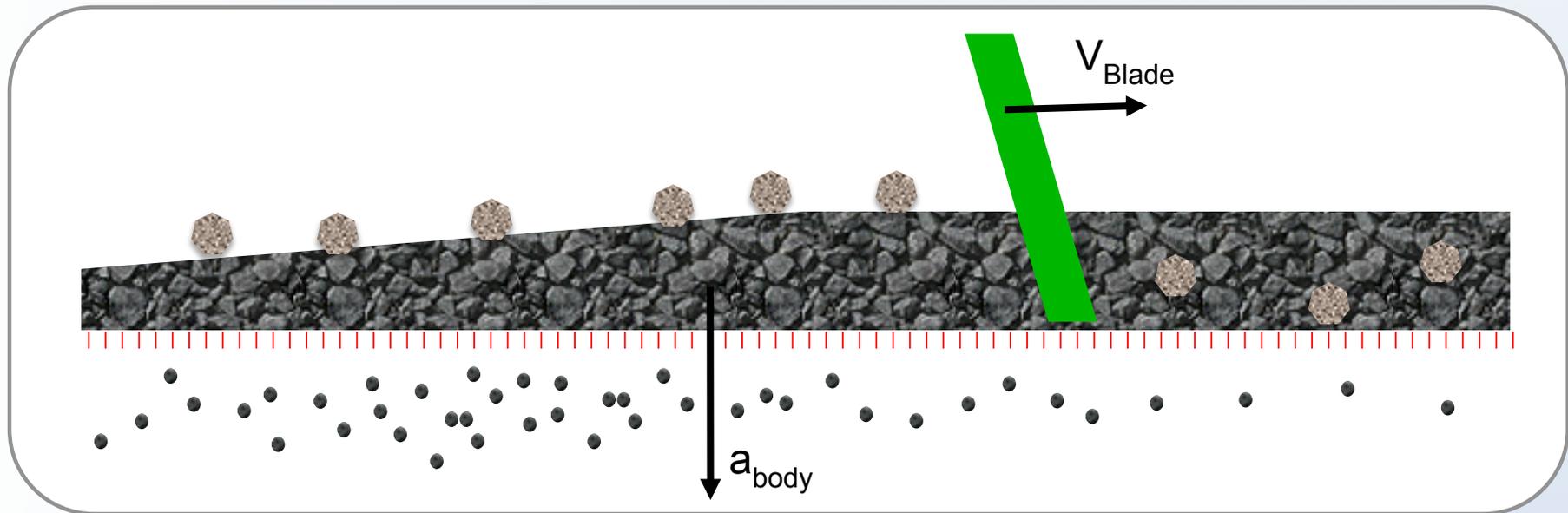
# Fluidized Bed flow becomes more cohesive in $\mu$ -g

- Williams (2006) showed that in reduced gravity the Geldart classification moved toward Class C, cohesive.
- Qian (2004) showed that centrifugal motion improved fluidization. Moving from Class C to A then B with increasing centrifugal force.



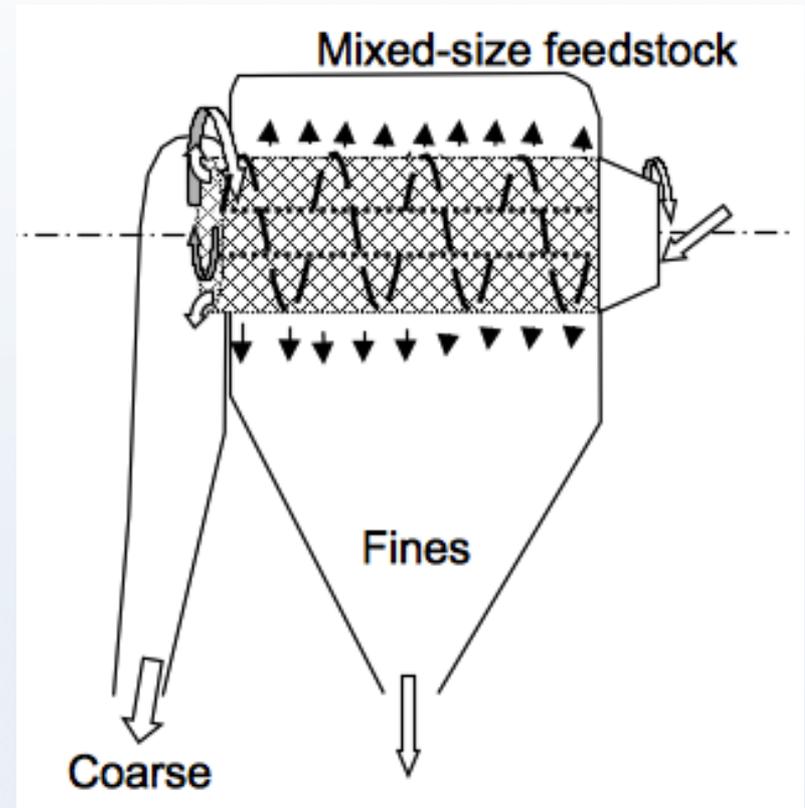
# Centrifugal Sieve Concept

- Centrifugal “force” drives particle flow
  - Gravity independent
- Shearing flow is induced by vibration or a moving blade
  - Larger particles naturally rise to the top in dry granular shear flow
  - Smaller particles fall downward

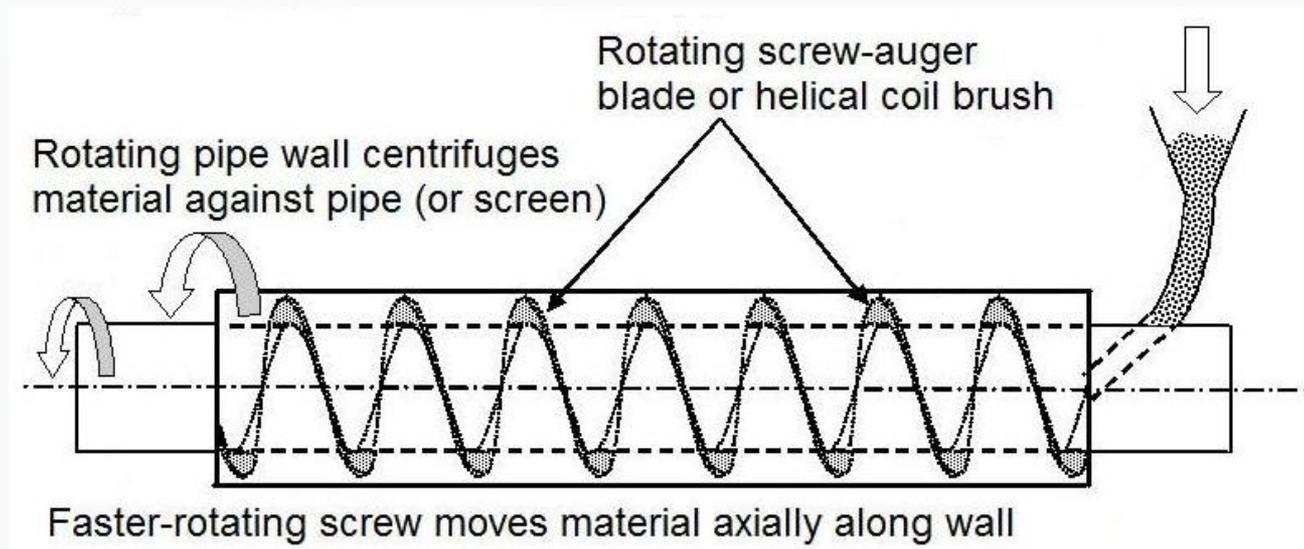


# Cylindrical screen and helical blade

- Helical blade rotates slightly faster than the cylindrical screen
  - Transport coarse material to outlet
  - Induces shear
  - Fines collected after passing through screen



# Rotating-wall conveyor



A rotating-wall, or centrifuging-pipe screw conveyor  
→ similar to an ordinary screw-conveyor

*except* the material is centrifuged to the pipe-wall where  
the screw moves it axially  
→ transport nearly independent of gravity-level

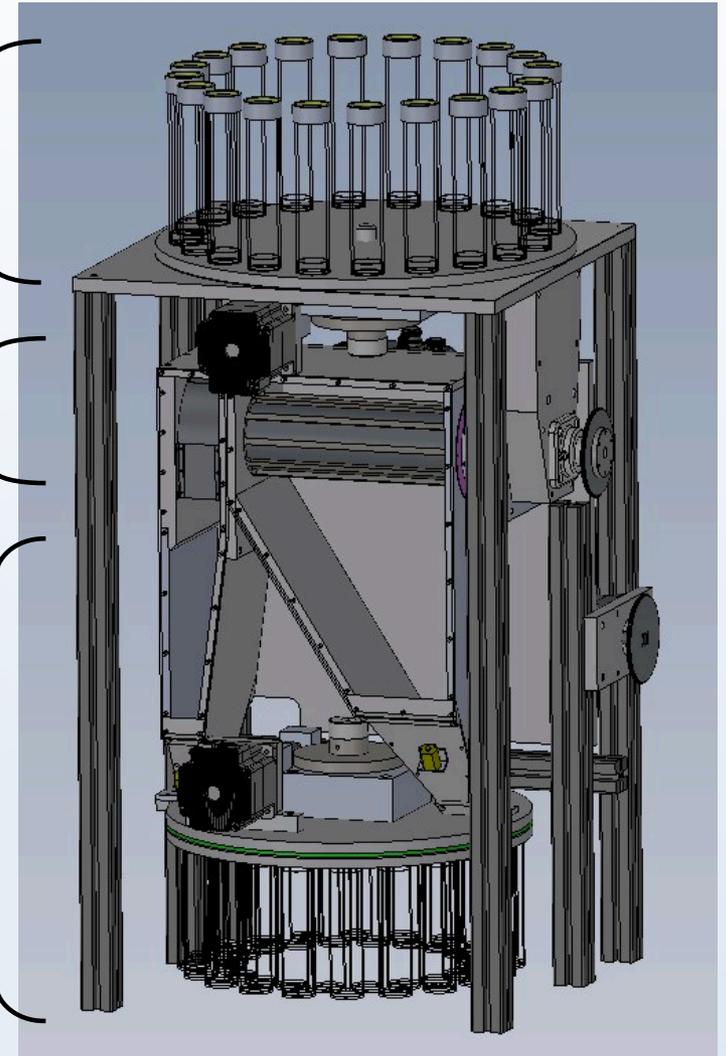
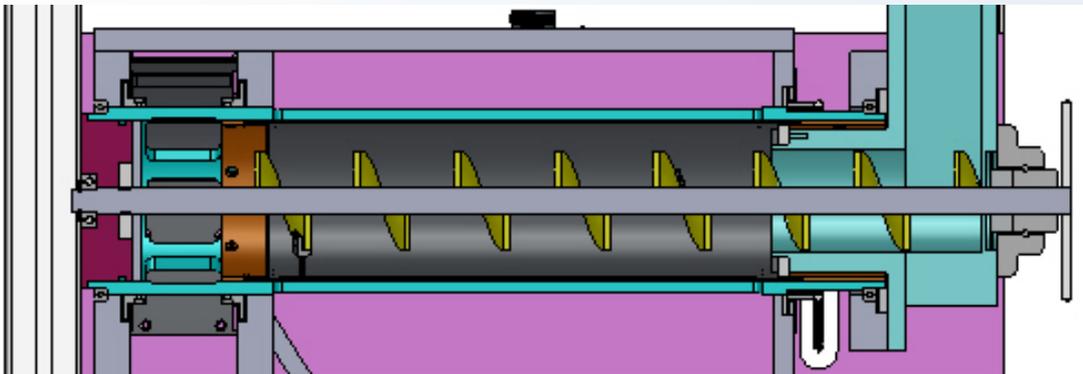


2 inch diameter cylinder at 300 rpm (2.5 g), Feeder Cone  
45° incline, Fine sand 200-600 micron diameter  
Equivalent to ~40 kg/hr



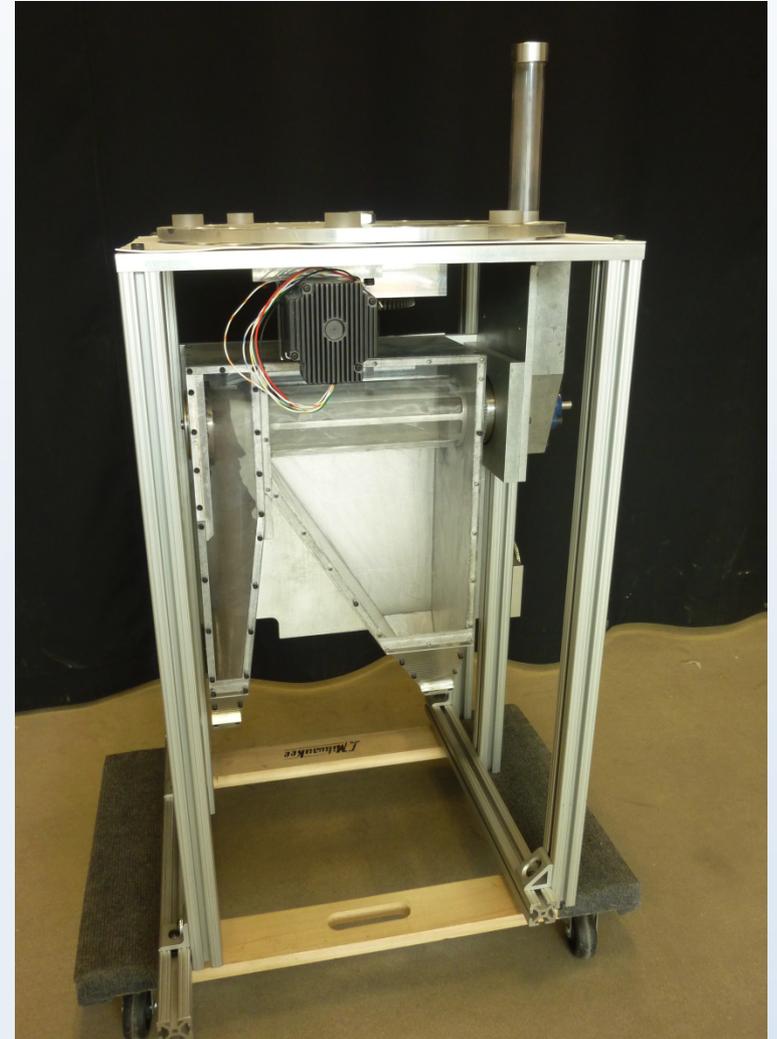
# Micro-g flight apparatus

- **Sample delivery carousel**  
20 sample delivery tubes  
delivery during high-g
- **Centrifugal Sieve**  
3 inch diameter sieve screen  
9 inch active length  
sieving/transfer during micro-g
- **Sample collection carousel**  
20 Fines collection tubes  
20 Overs collection tubes  
collection during high-g



# Built and tested in 1-g

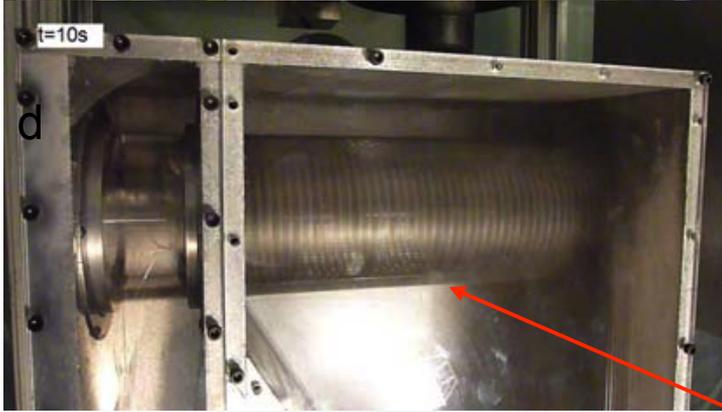
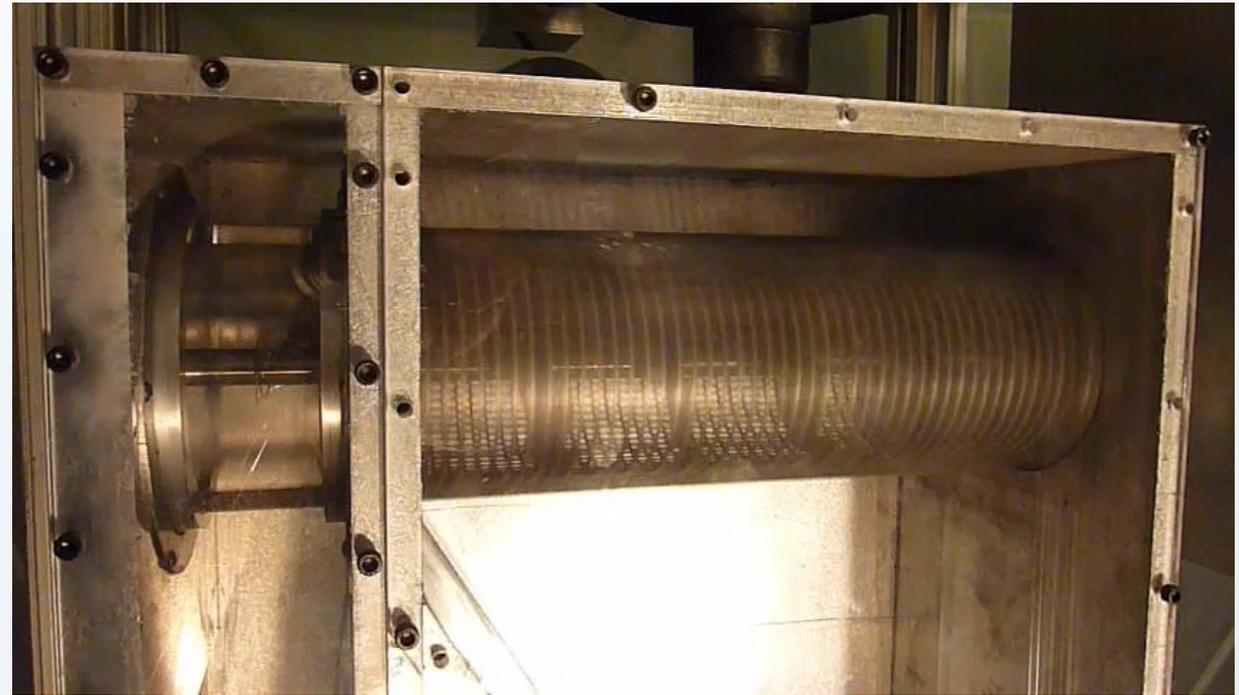
- ~85% built in phase 1. Collection carousel not built
- Tested sieving and dispensing in 1g with 4.6 mm and 100  $\mu\text{m}$  screens.
- Tested from 1.5 to 3g<sub>o</sub> (185 to 270 rpm, blade +60rpm)



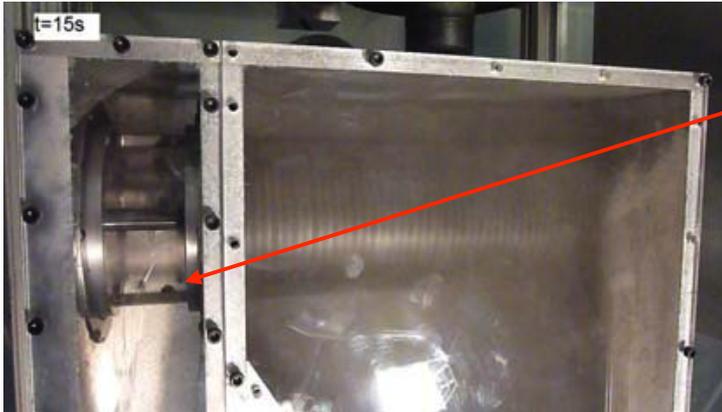
# Sieving >4.6mm from (JSC-1a + 5mm pebbles)



Fines begin to come through the screen



Fines exit further



Large fragments in the overs chute

Fines envelope the entire fines chute

Input:

400g JSC1a

+ 40g >5mm, pre-screened

Output:

Overs: 40g

Fines: ~398g

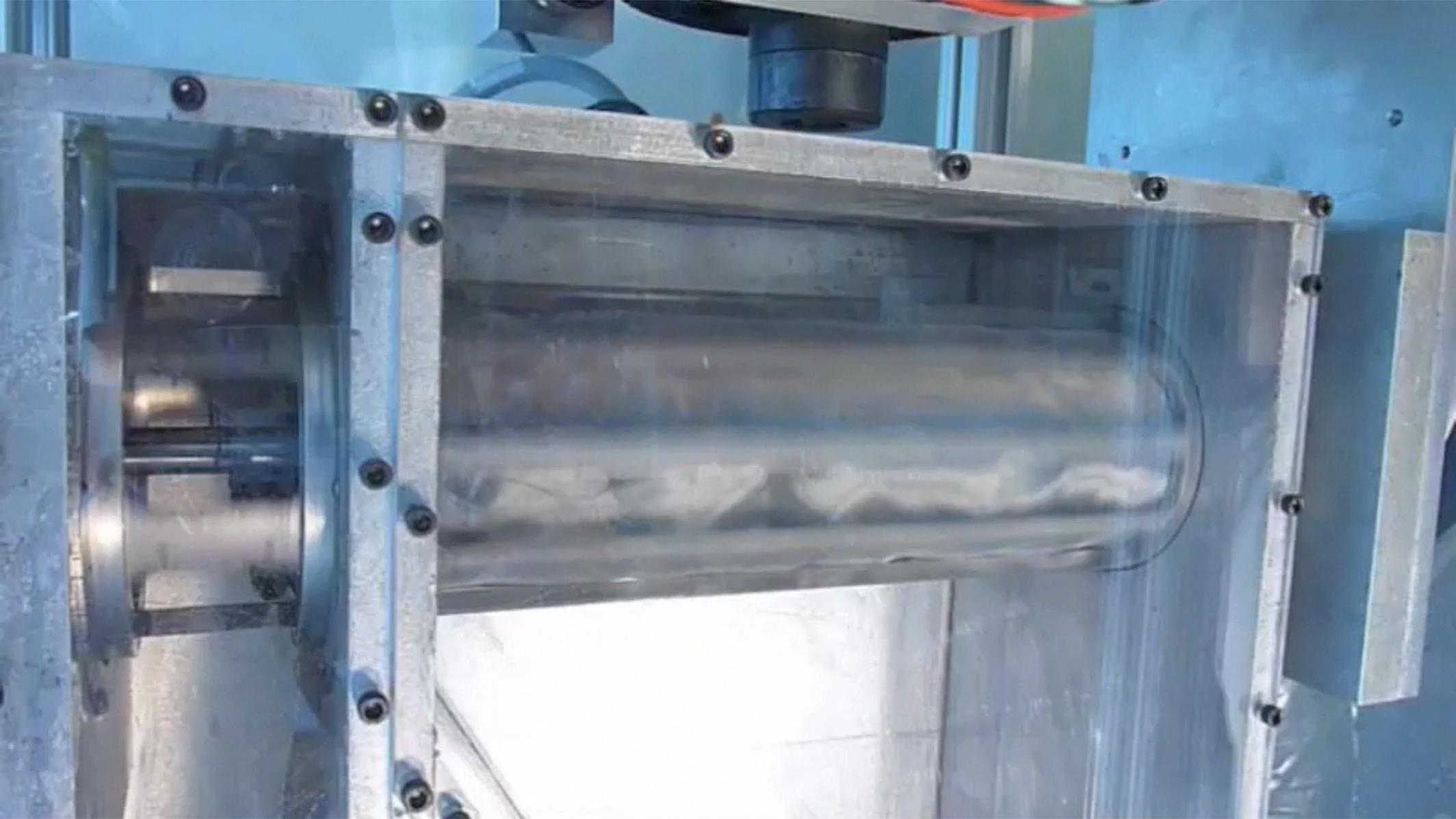
30 second test

Rate > 50 kg/hr

# 100 $\mu\text{m}$ screen



# 100 $\mu\text{m}$ screen with JSC-1a



# JSC-1a sieving

• Input: 400g JSC-1a

• Output:

- Fines <100  $\mu\text{m}$  213 g (55%)
  - Overs >100  $\mu\text{m}$  175 g (45%)
- ~30 second test  
Rate > 50 kg/hr

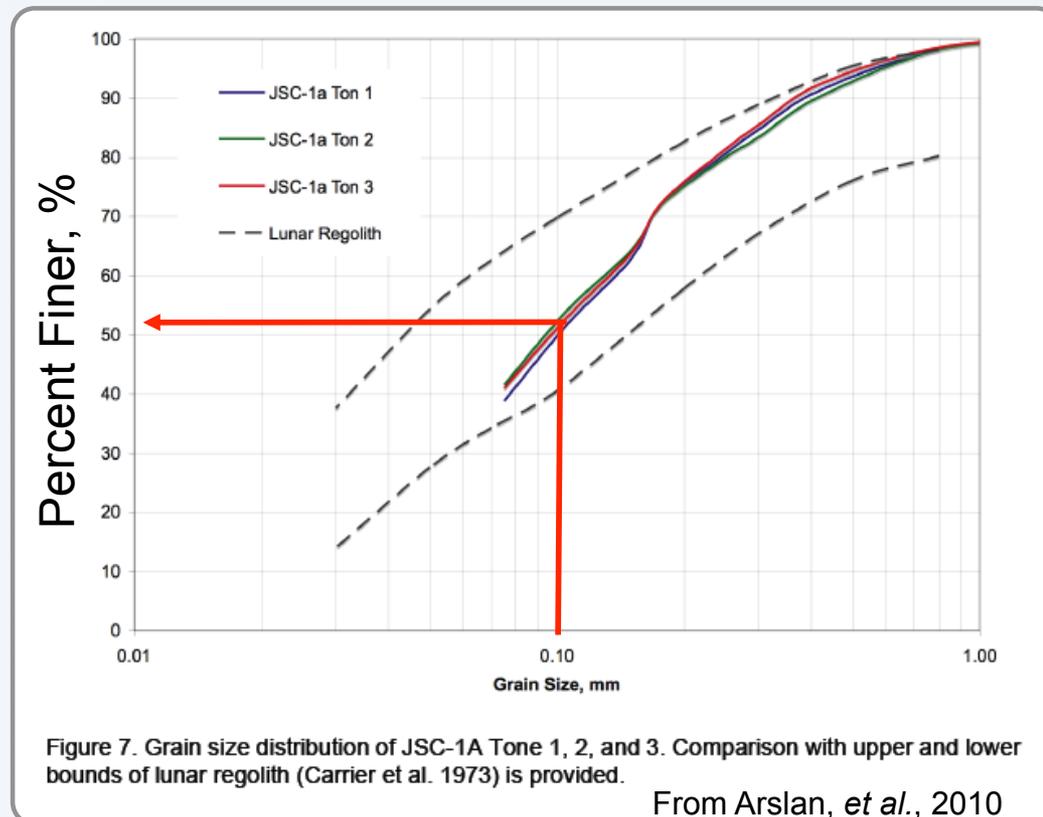
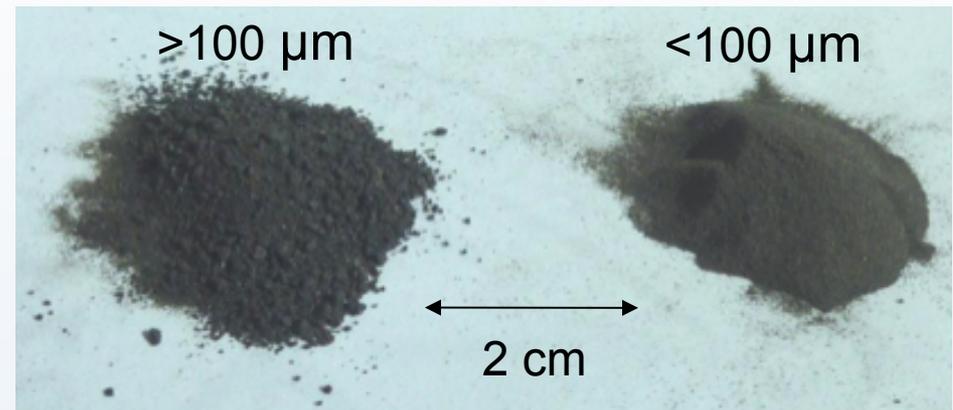
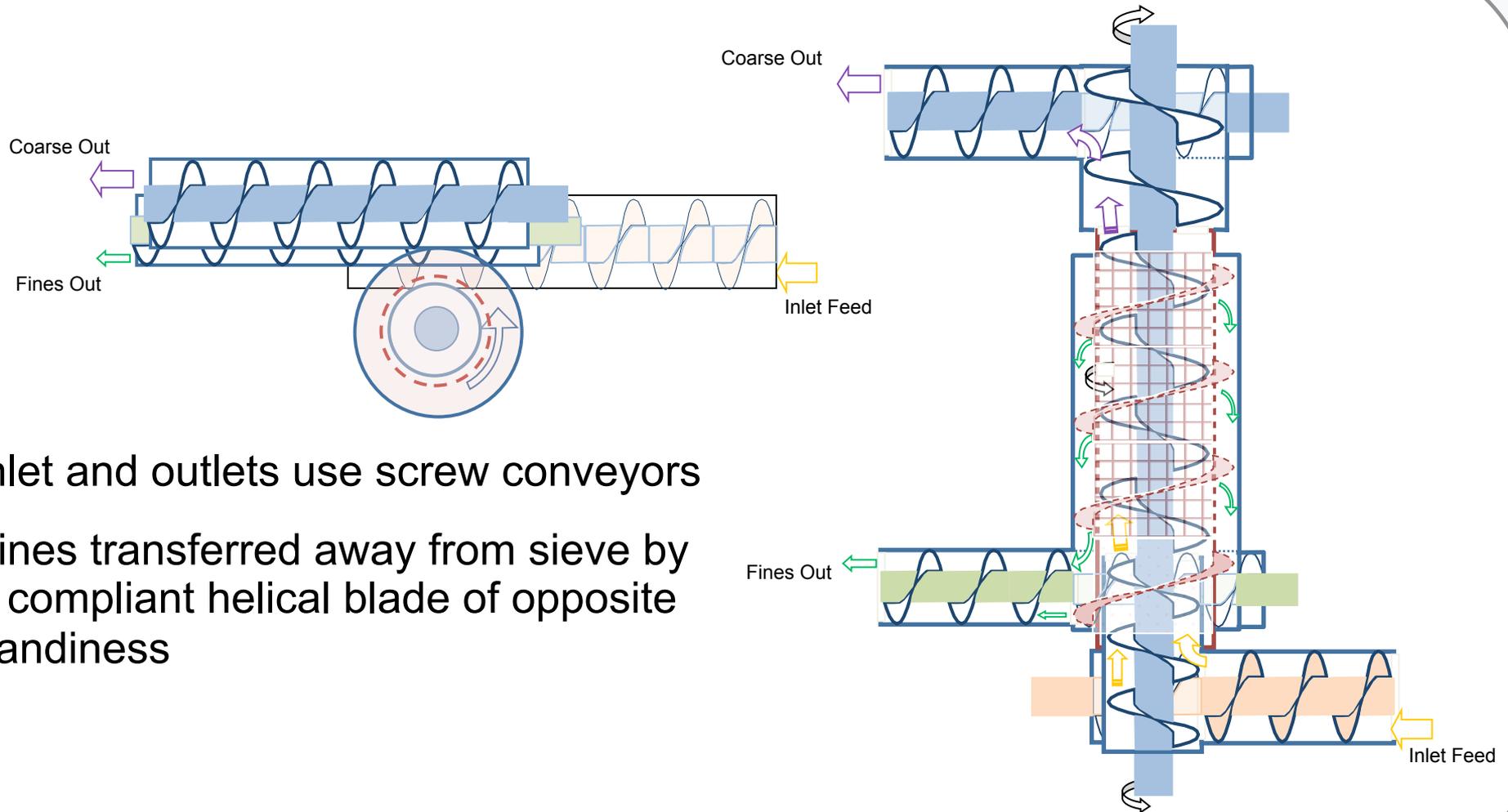


Figure 7. Grain size distribution of JSC-1A Tone 1, 2, and 3. Comparison with upper and lower bounds of lunar regolith (Carrier et al. 1973) is provided.

From Arslan, *et al.*, 2010

# Micro-gravity capable centrifugal sieve



Inlet and outlets use screw conveyors

Fines transferred away from sieve by a compliant helical blade of opposite handiness

# Next Steps for the Centrifugal Sieve

- Improve TRL
- Micro-g and vacuum tests
- Optimize operation
- Develop the fully micro-gravity-capable version

# Conclusions

- Sieving technology is fundamental to many ISRU processes.
- Fine granular material behaves as a more cohesive material in low gravity and micro-gravity.
- Centrifugal sieve successfully separated  $>5$  mm material from JSC-1A and size split JSC-1A at  $100\mu\text{m}$ . Rate above 50 kg/hr.
- Good beneficiation method for rapid segregation of cohesive granular material less than 1 cm size. Particularly suited for when pneumatic systems are not feasible.
- Centrifugal systems should be used for many more applications, such as for material transport and fluidized bed processors.

Thanks for listening

Questions?